

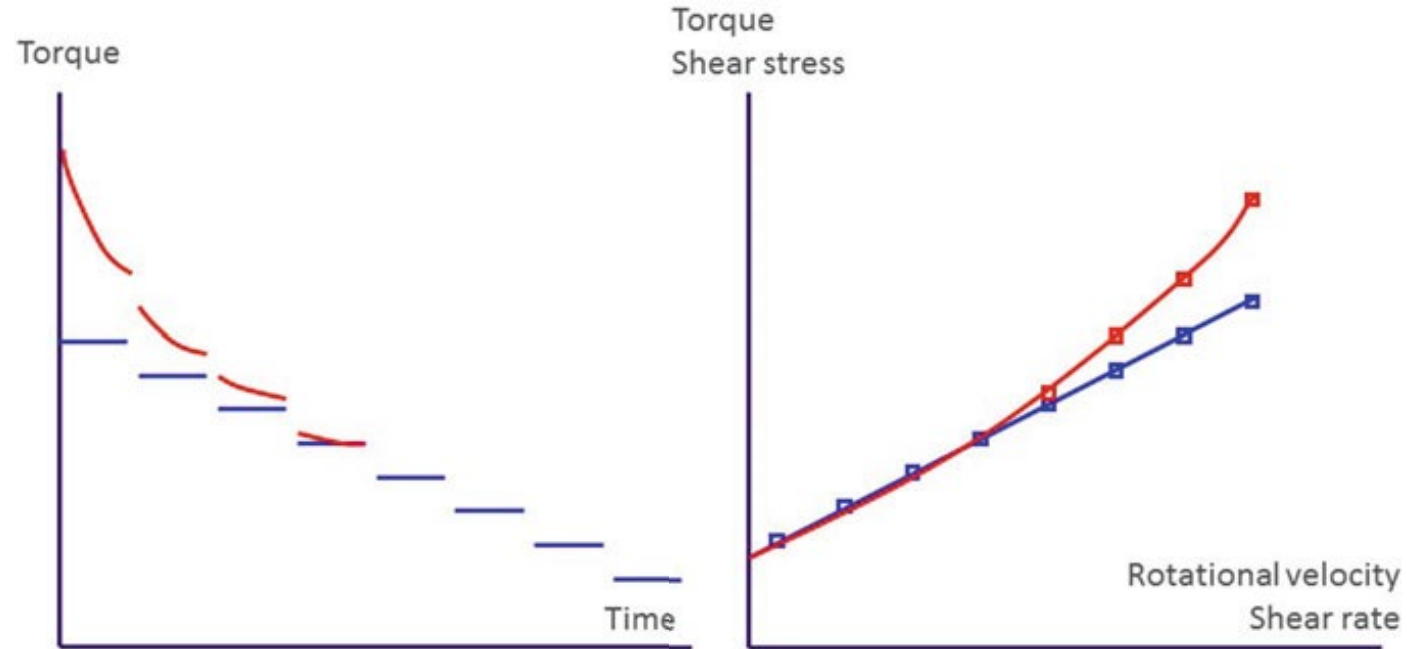


Wide-Gap Rheometer Step-Profile Analysis for Thixotropy Assessment and Numerical Criteria for Equilibrium and Flow Model Choice

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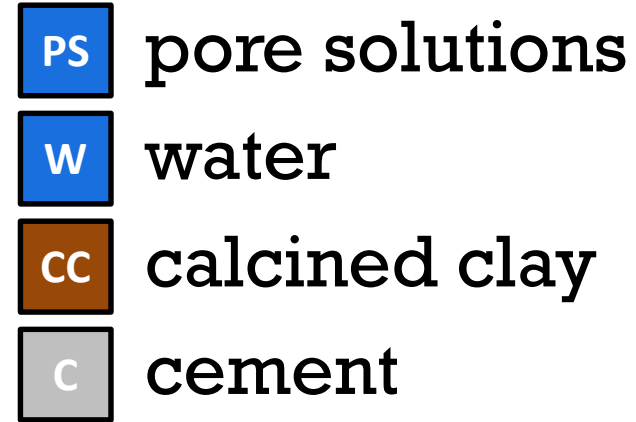
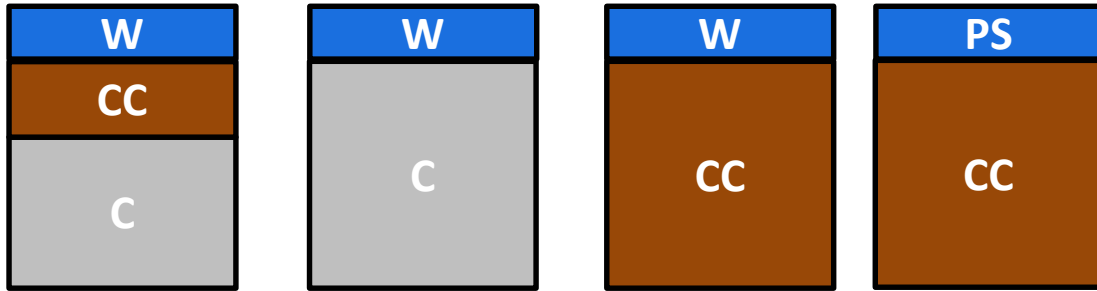
Who is determining equilibrium by visual inspection?

Methods

Data set

~275 rheometer runs

Different ratios of



water/binder ratio: 0.4-1.2

w/ and w/o



At different time intervals



Rstudio

Equilibrium

Rheometer profile suggestions

pre-shear at highest shear rate

downward ramp

~30s per step

State of the Art Report
Measuring Rheological Properties of Cement-based Materials: State-of-the-Art Report of the RILEM Technical Committee 266-MRP

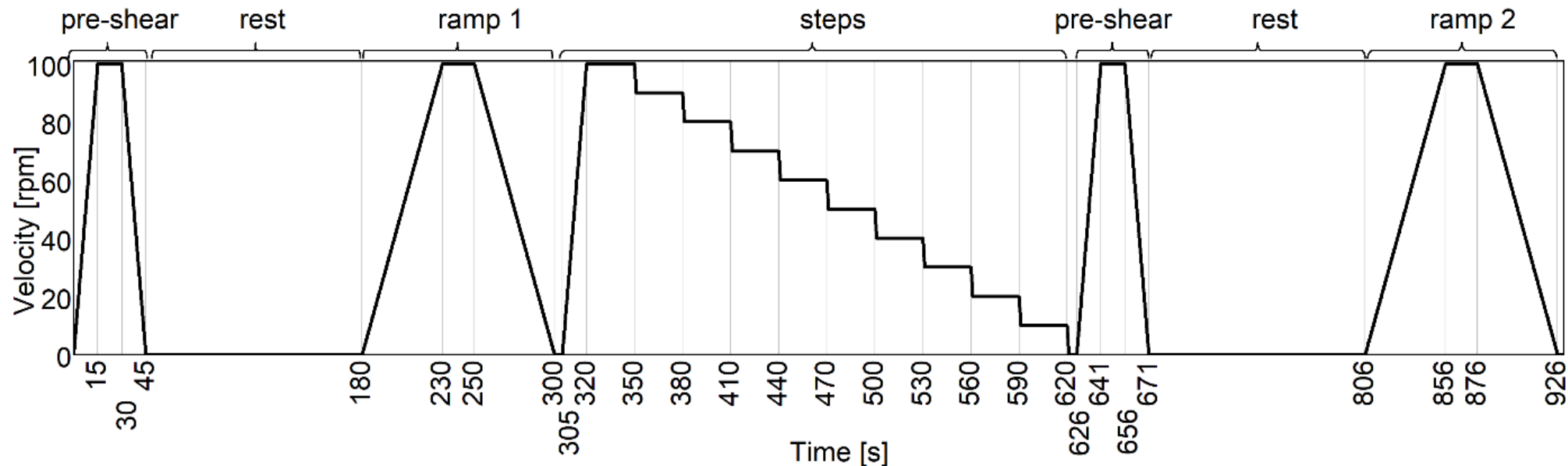
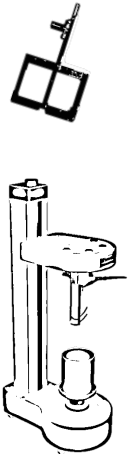


methods

rheometer – Viskomat NT

Sampling frequency ~ 9.9125 Hz

All data apparent rheological values (viscosity, yield stress etc!!)



Equilibrium

Integrity of data

Sedimentation

Plug flow

...

...

...



Viskomat NT



Viskomat XL

Schau in den Topf

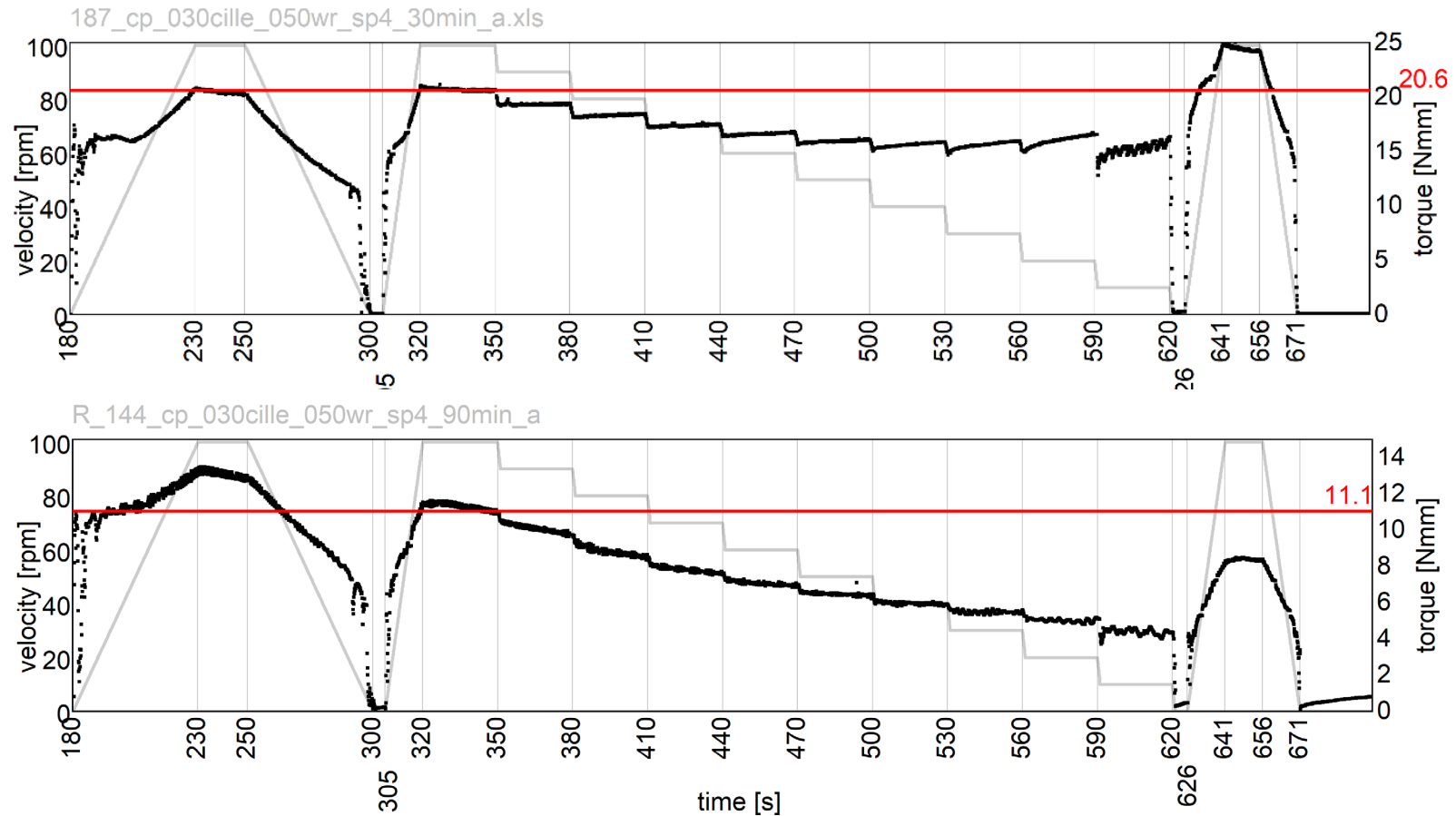
Look in the cup

Institute for Construction Materials

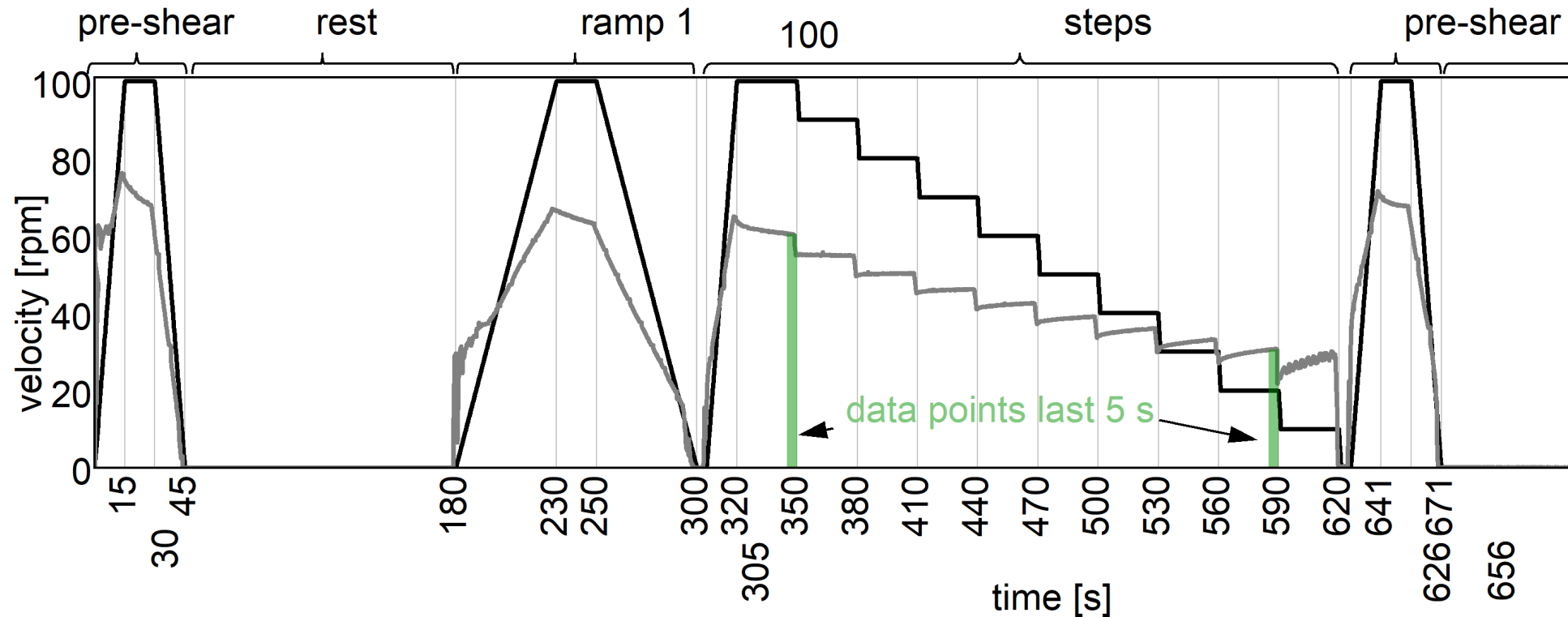
Equilibrium

Max RPM factor

$0.9 < x < 1.1 \rightarrow \sim 30$ measurements



Equilibrium Step analysis



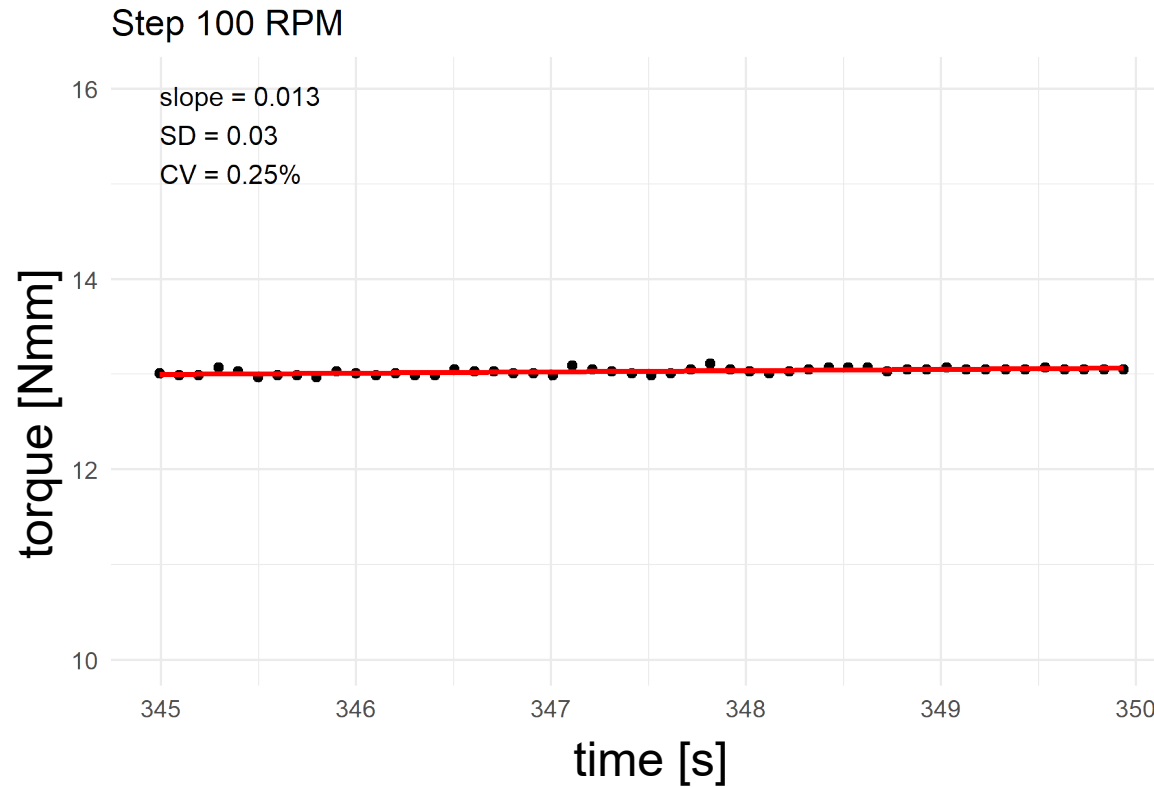
Equilibrium

Step analysis



$$1 \% < \text{Coefficient of variation} = \frac{\text{standard deviation}}{\text{mean average (ME)}}$$

$$|0.05| \frac{\text{Nmm}}{\text{s}} < \text{slope incline}$$

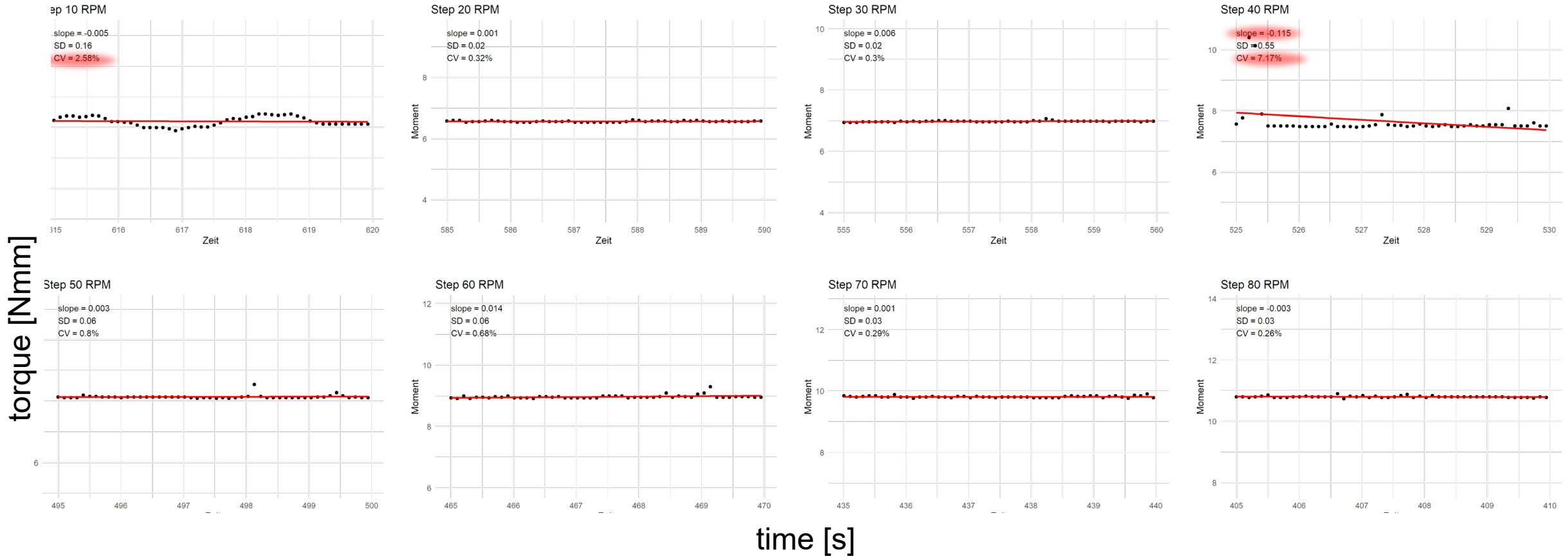


Equilibrium Step analysis



$$1 \% < \text{Coefficient of variation} = \frac{\text{standard deviation}}{\text{mean average (ME)}}$$

$$|0.05| \frac{\text{Nmm}}{\text{s}} < \text{slope incline}$$





Choice of profile

Integrity of data (particle migration)

Max RPM check

Slope incline / variation coefficient

Minimum of 5 data points

} need to be fine tuned
to the data set

Flow model choice

Flow models used



Bingham (BH)

linear

$$\tau = \tau_0 + \mu_p \dot{\gamma}$$

Modified Bingham (MB)

quadratic

$$\tau = \tau_0 + \mu_p \dot{\gamma} + c^* \dot{\gamma}^2$$

Herschel-Bulkley (HB)

non-linear power-law

$$\tau = \tau_0 + K \dot{\gamma}^n$$

τ_0 yield stress

μ_p viscosity

$\dot{\gamma}$ shear rate

c MB factor nonlinearity

(shear thinning $< 0 <$ shear thickening)

K HB viscosity factor

n HB Flow behavior index

(shear thinning $< 1 <$ shear thickening)



$$\tau = \tau_0 + K\dot{\gamma}^n$$

Boundaries

$$\tau_0 > 0$$

$$K > 0$$

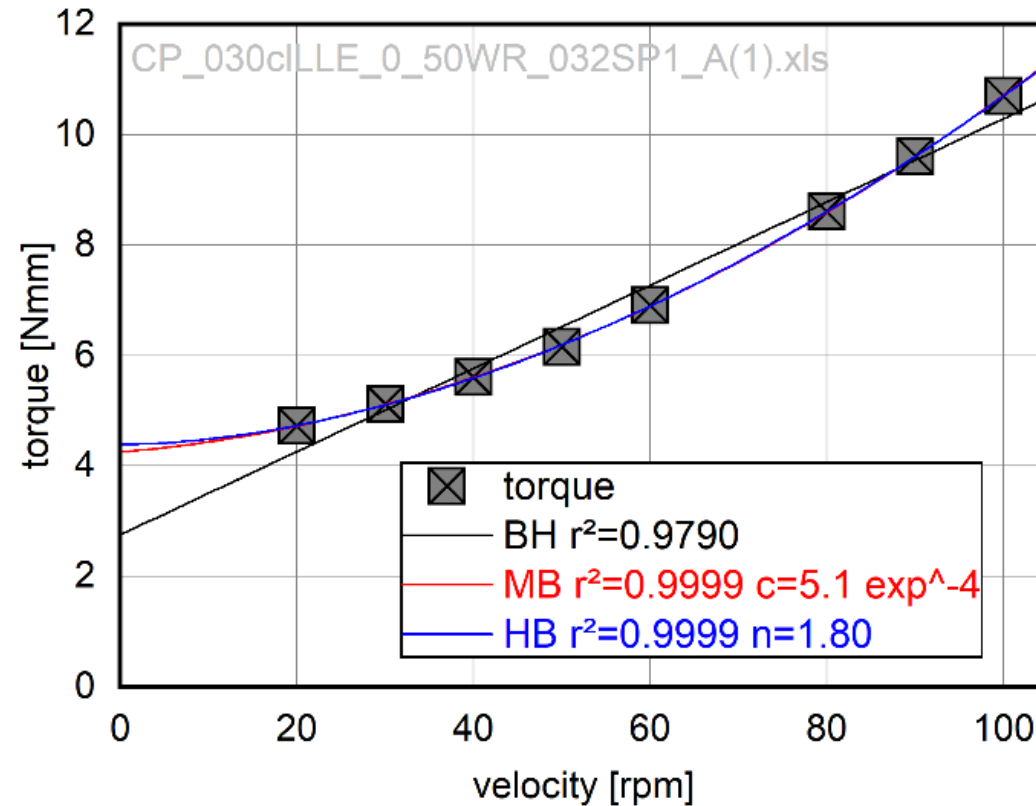
$$0.5 \leq n \leq 2.3$$

Seeding value for τ_0 = Bingham τ_0

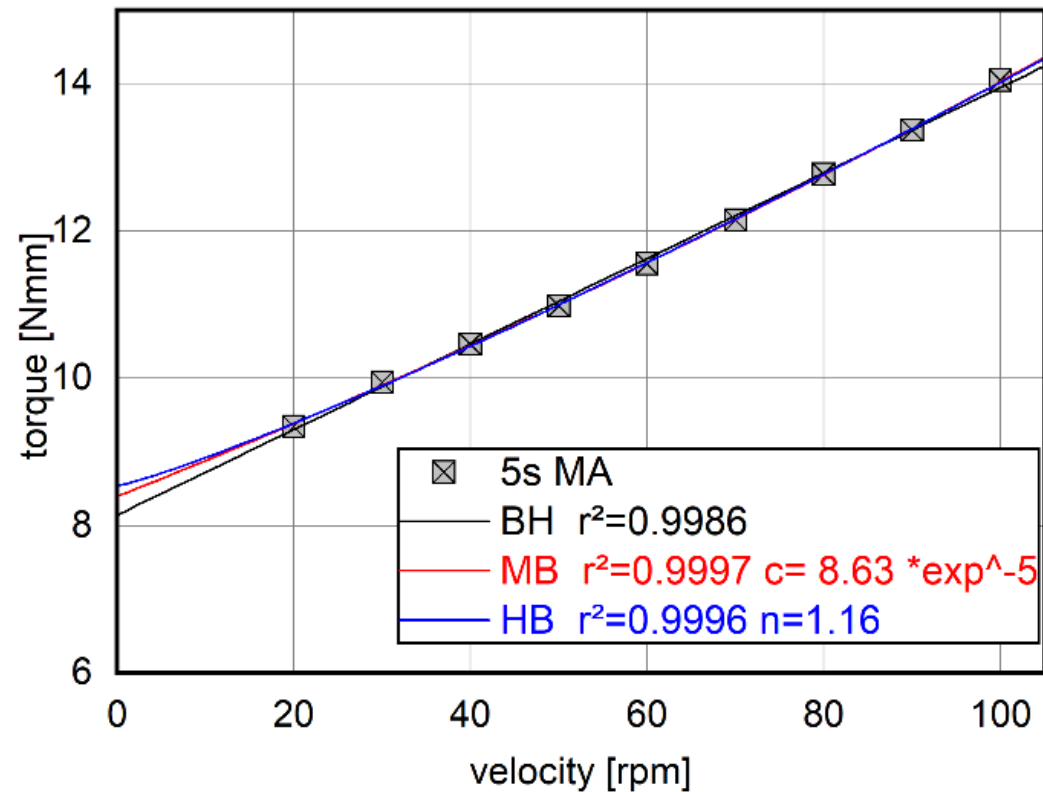
Seeding value for K = Bingham μ

Seeding values for n [0.7; 0.9; 1.0; 1.1; 1.5]

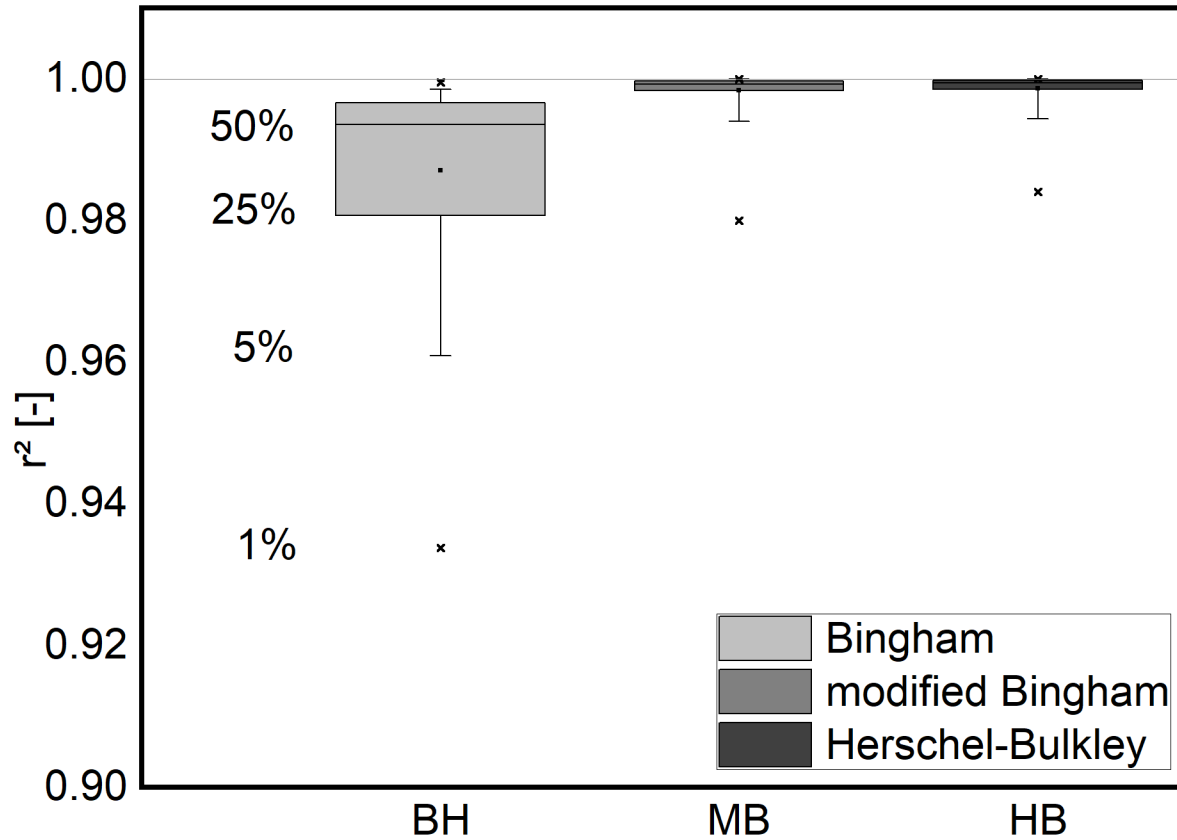
Flow Model Choice by hand – Example 1



Flow Model Choice by hand – Example 2



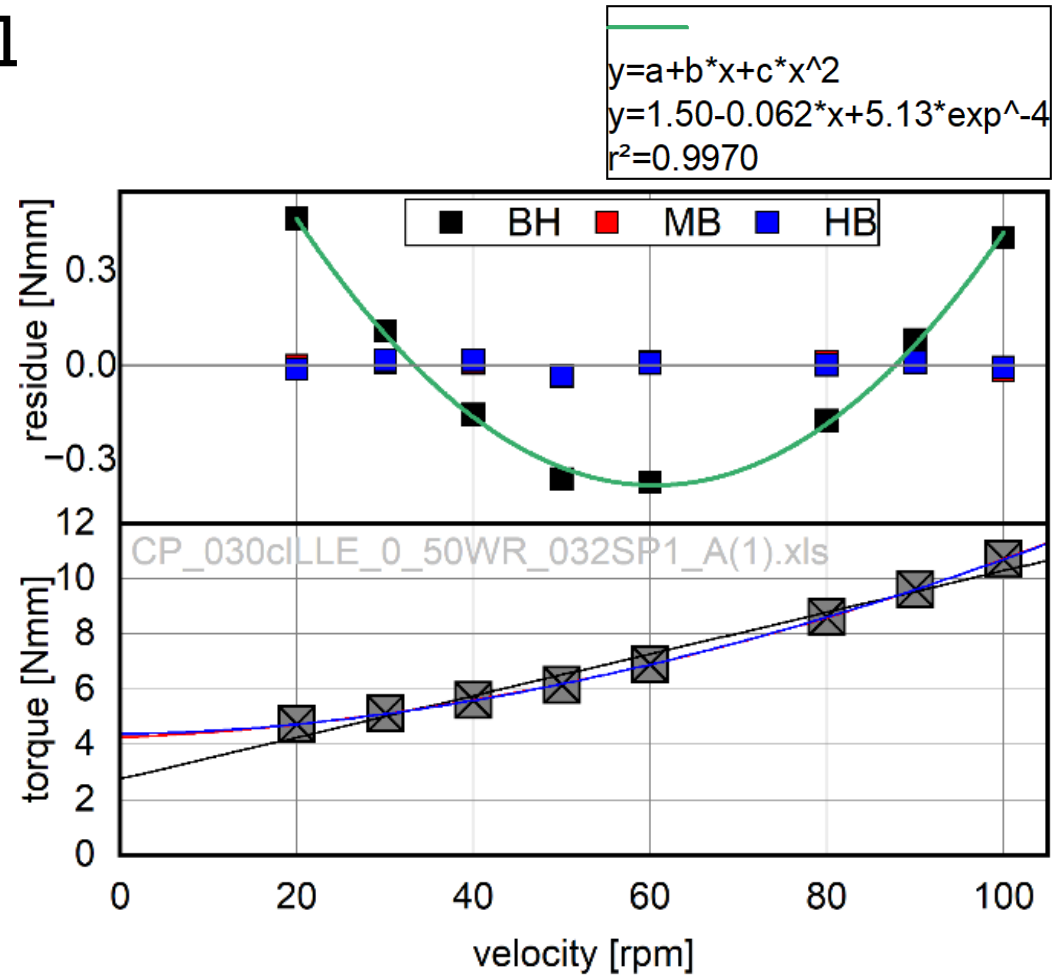
Flow model choice



~77 data sets have $n > 1.5$
BH $r^2 \sim 0.95$

Flow model choice

Residue analysis 1

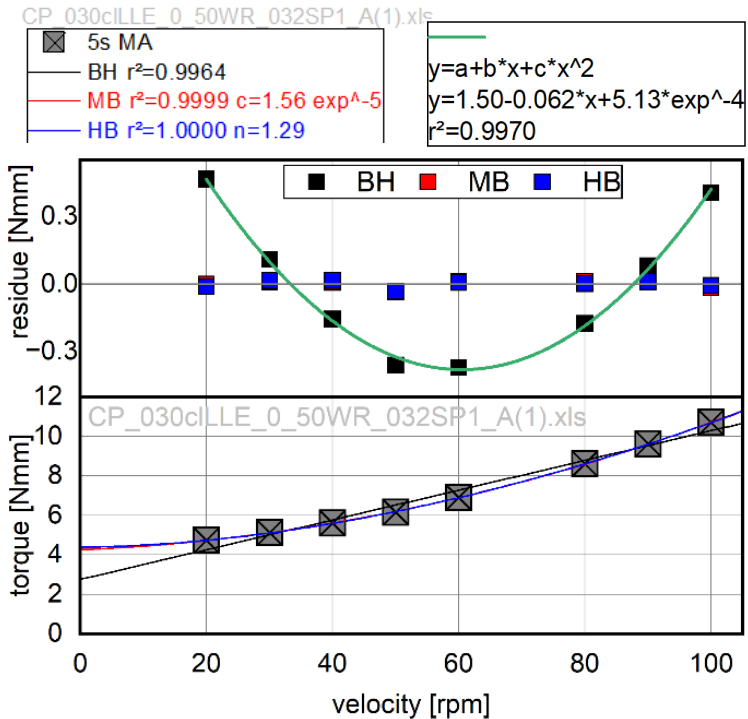


Flow Model Choice

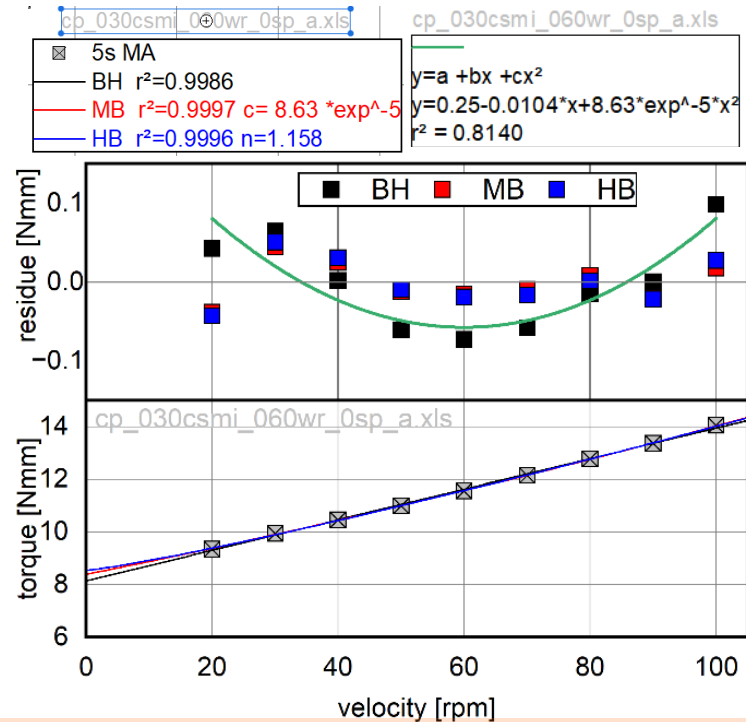
Residue



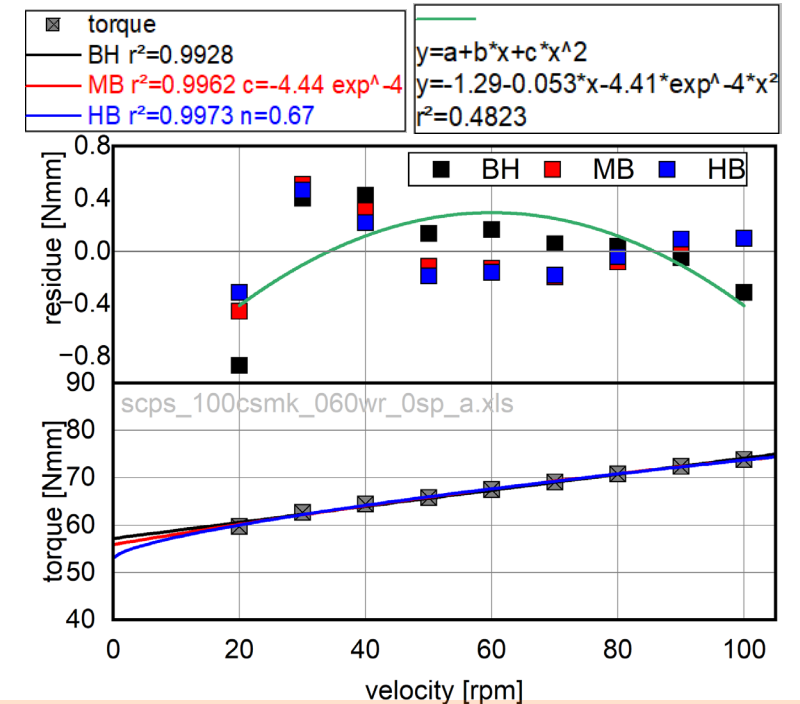
Example 1



Example 2



Example 3



2nd degree polynomial fit on bingham residue.
linear fit $<r^2=0.5<$ non linear fit

What can I help with?

+ Ask anything

📖 Organization knowledge

ChatGPT can make mistakes. OpenAI doesn't use UniBwM-ChatGPT EDU workspace data to train its models.

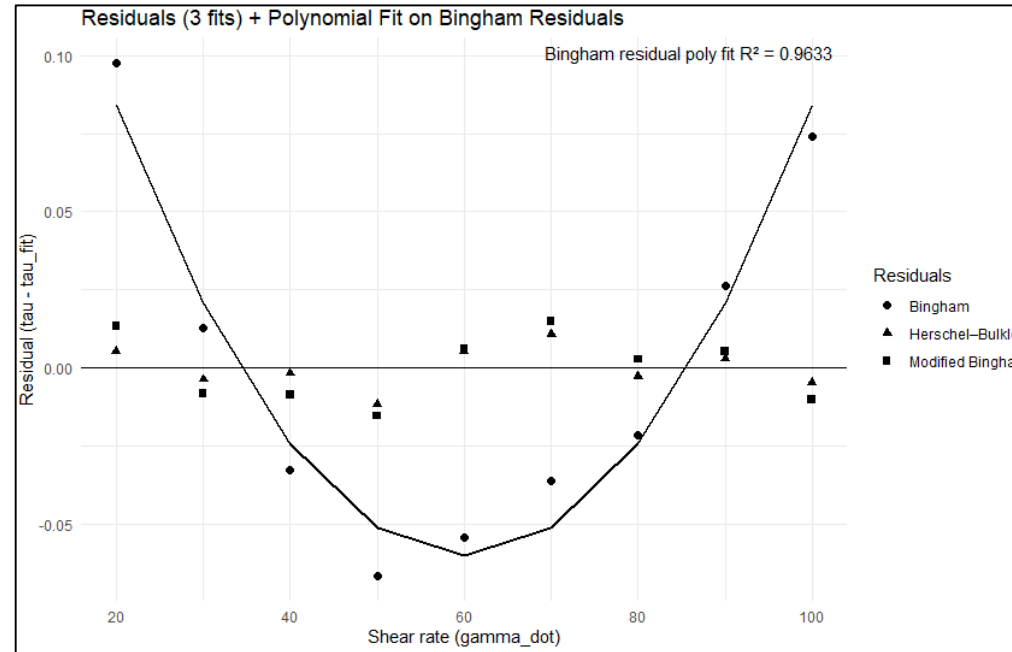
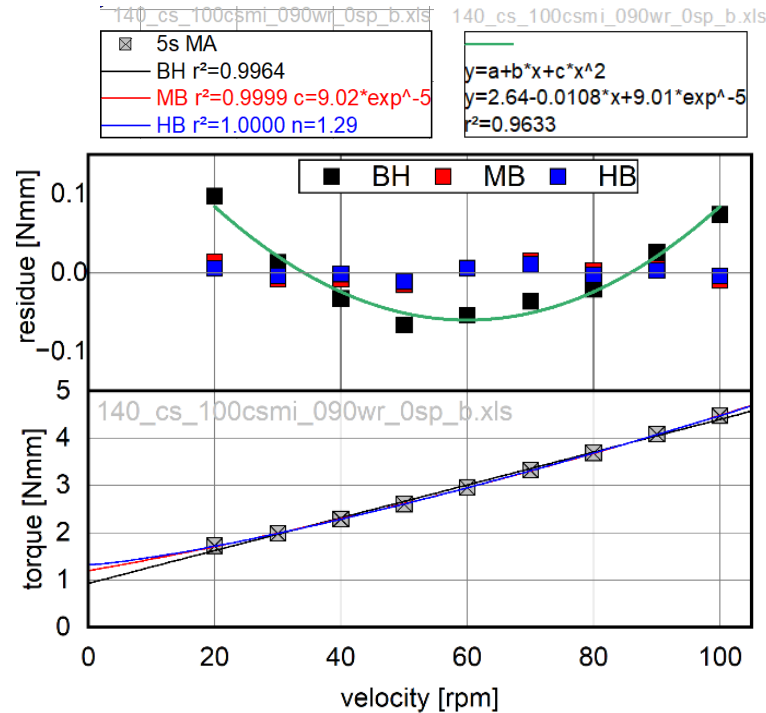
Good morning chatgpt

its fine. thank you for asking. how are you?

I need some help with rheology data. I have an excel sheet with the following data format: and i need an anylsis on that.

1. i need bingham, mod bingham and herschel bulkley fit on these values. I need residues on the previous three fits. and i need a second degree polynomial fit only on the bingham residues with the according r^2 . this needs to be displayed in two graphs. 1 the three fits with their values and raw data and second the three residues plus polynomial fit with r^2 please write me an r studio script. the excel sheet name is "schleibi_conference_140"

Flow model choice



$$BH = 0.9336 + 0.0346 * x$$

$$MB = 1.1982 + 0.0239 * x + 9.01 * 10^{-5} * x^2$$

$$HB = 1.3257 + 0.00817 * x^{1.293}$$

==== FIT RESULTS ====

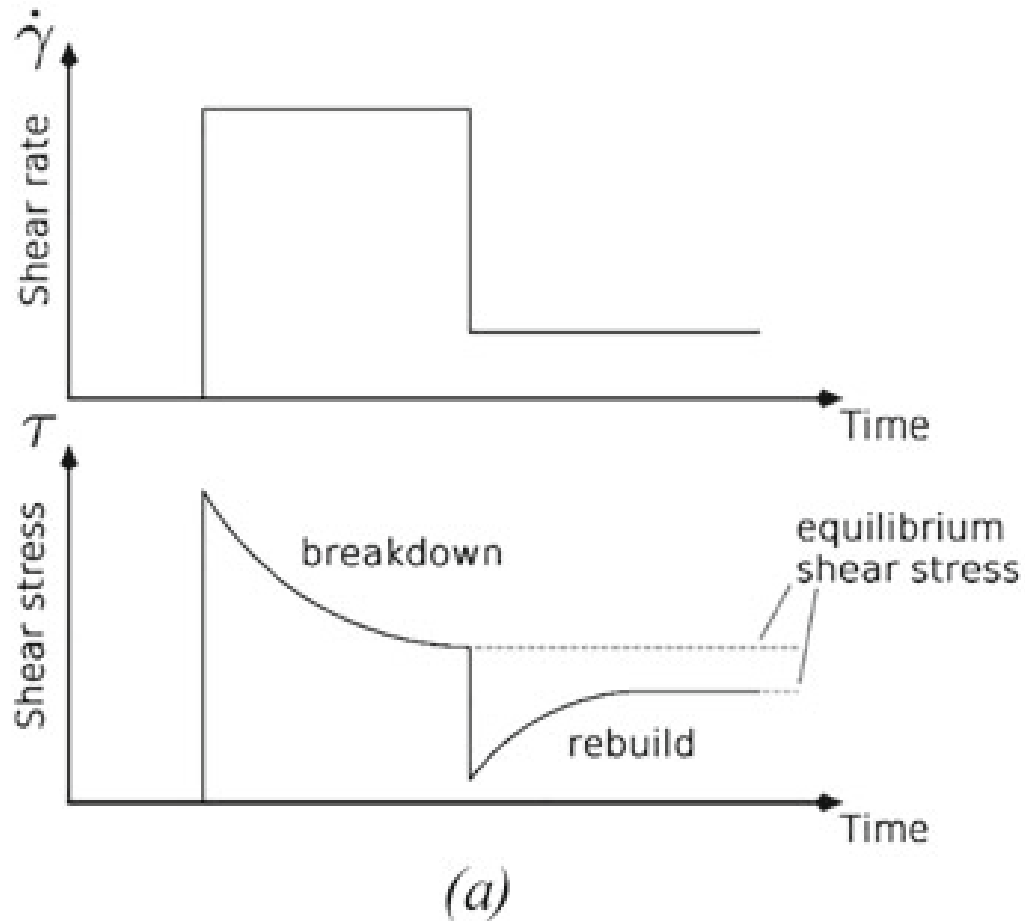
Bingham: $\tau = 0.933684 + 0.034689 * \gamma$

Modified Bingham: $\tau = 1.198150 + 0.023870 * \gamma + 0.000090 * \gamma^2$

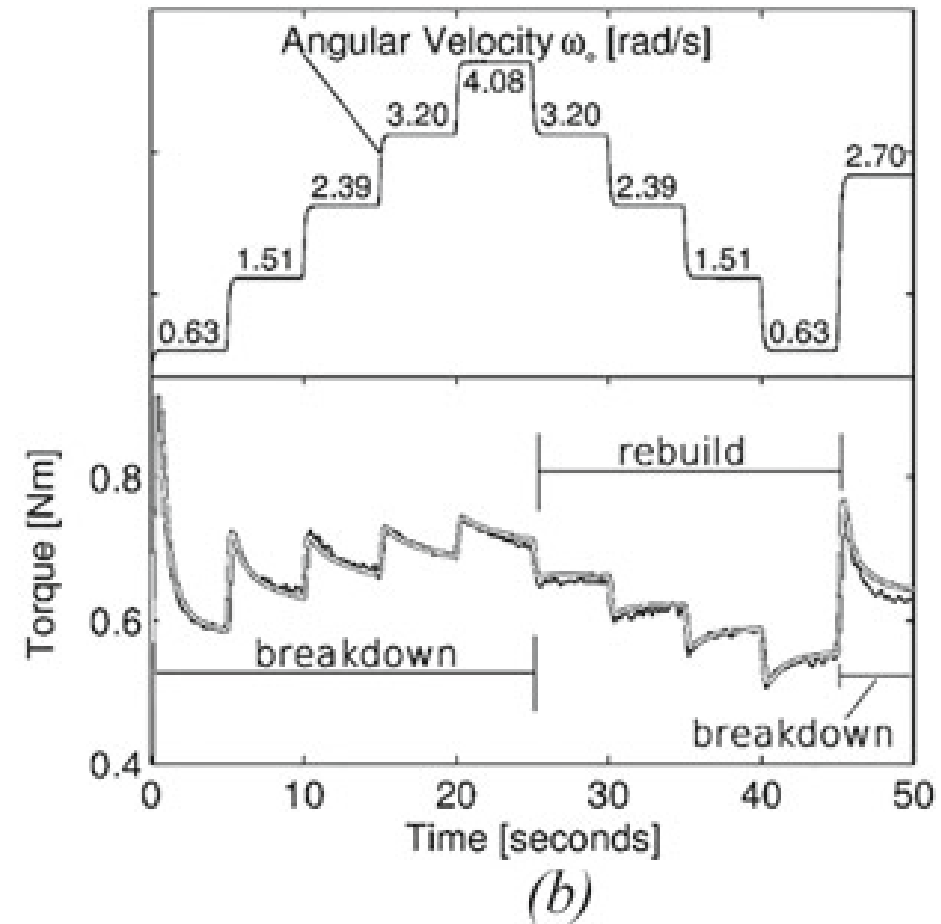
Herschel-Bulkley: $\tau = 1.325735 + 0.008177 * \gamma^{(1.293244)}$

Polynomial on Bingham residuals: $R^2 = 0.963343$

Thixotropy on a step profile



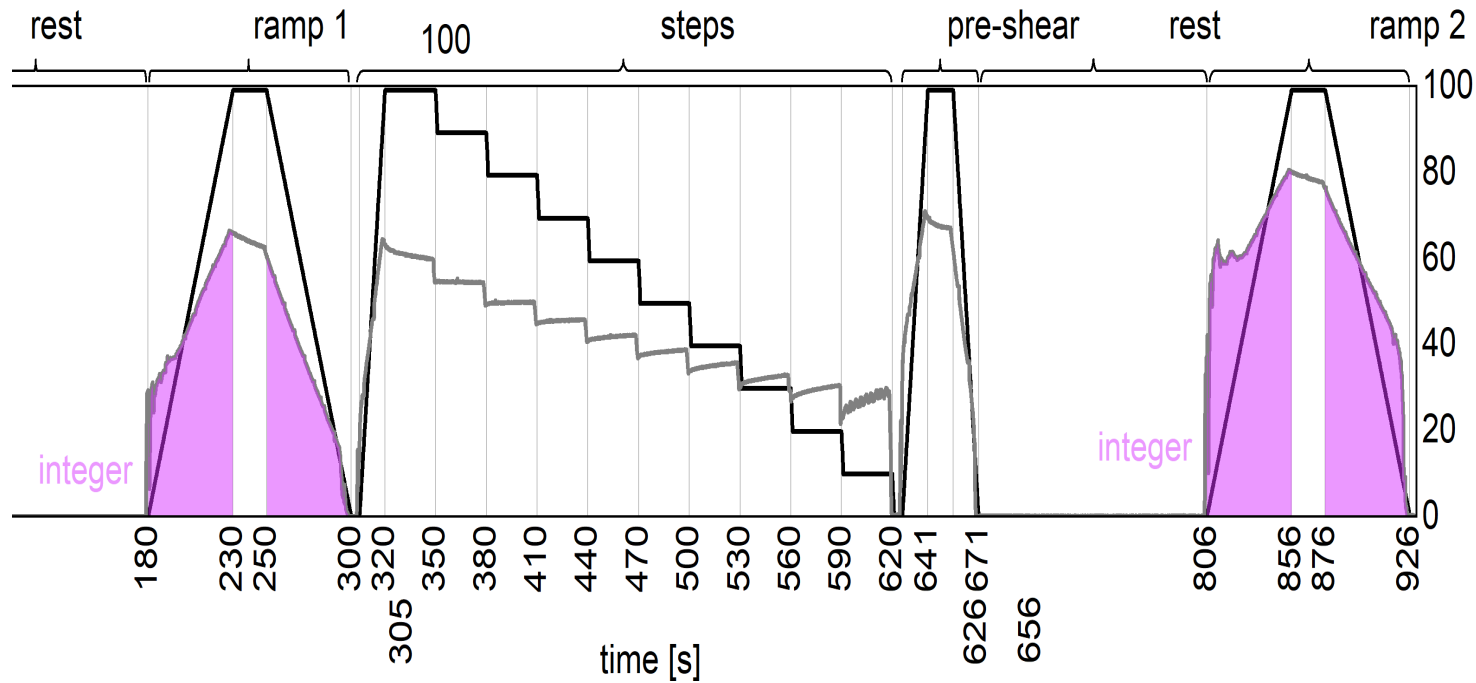
(Sonebi & Feys, 2024)



(Wallevik, 2009)

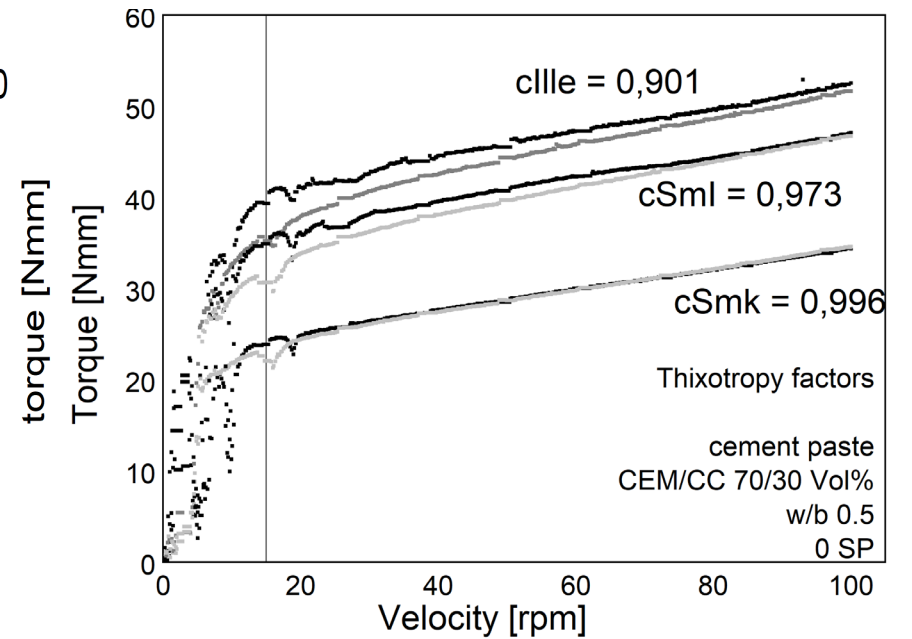
Thixotropy on a step profile

hysteresis



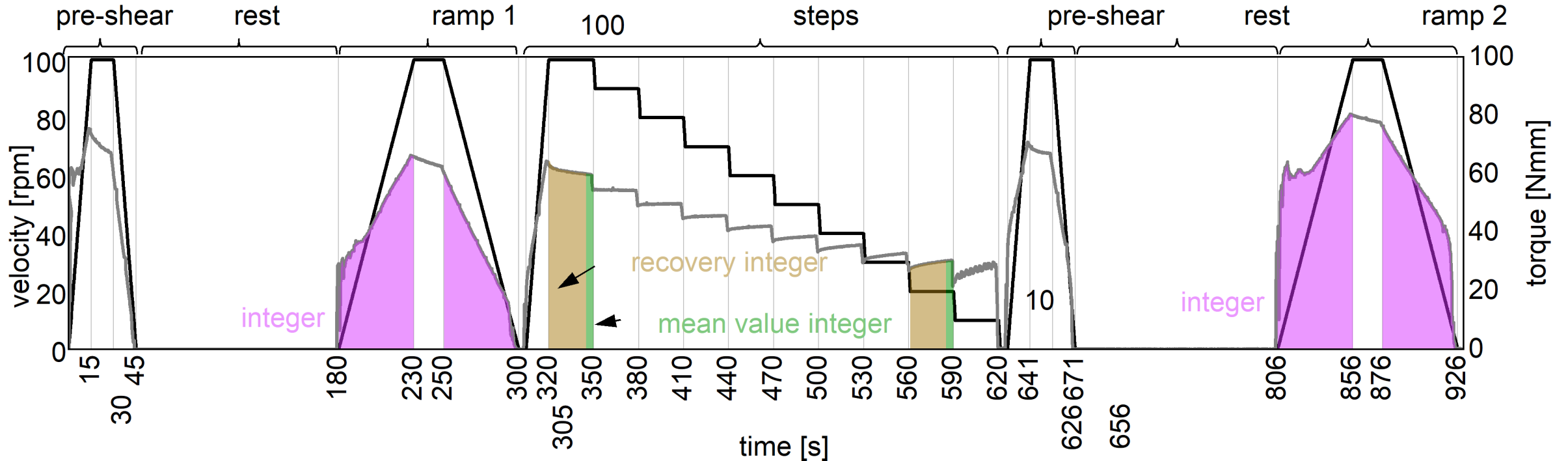
Thixotropy factor 1 (Thix 1)

Thixotropy factor 2 (Thix 2)



Thixotropy on a step profile

Inertia and recovery value



$$value = \frac{\text{recovery integer: } 30s}{\text{mean value integer: } 5s} * 100 - 100 [\%]$$

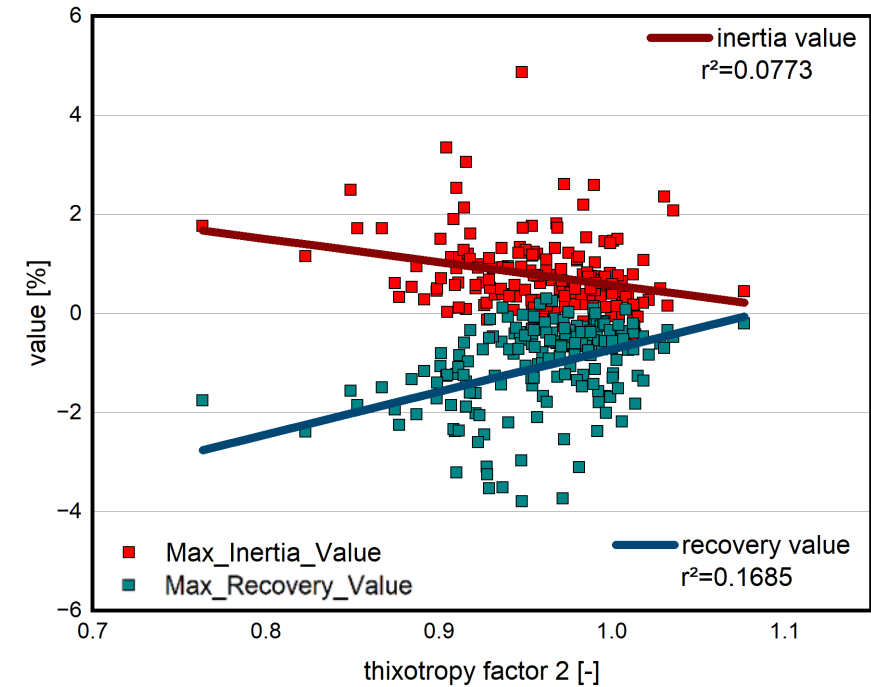
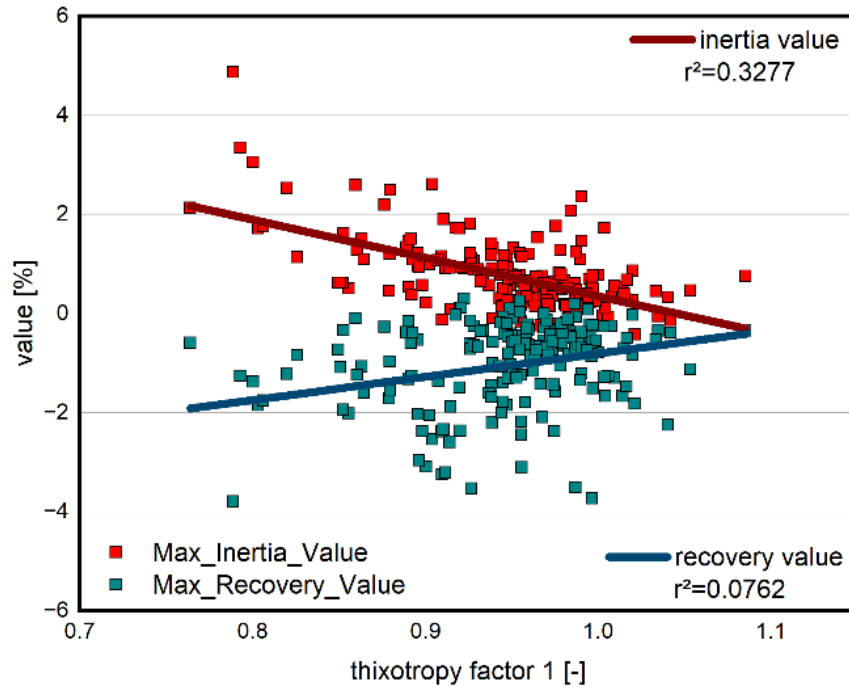
Maximum (values[10steps])

value > 0 -> inertia value

value < 0 -> recovery value

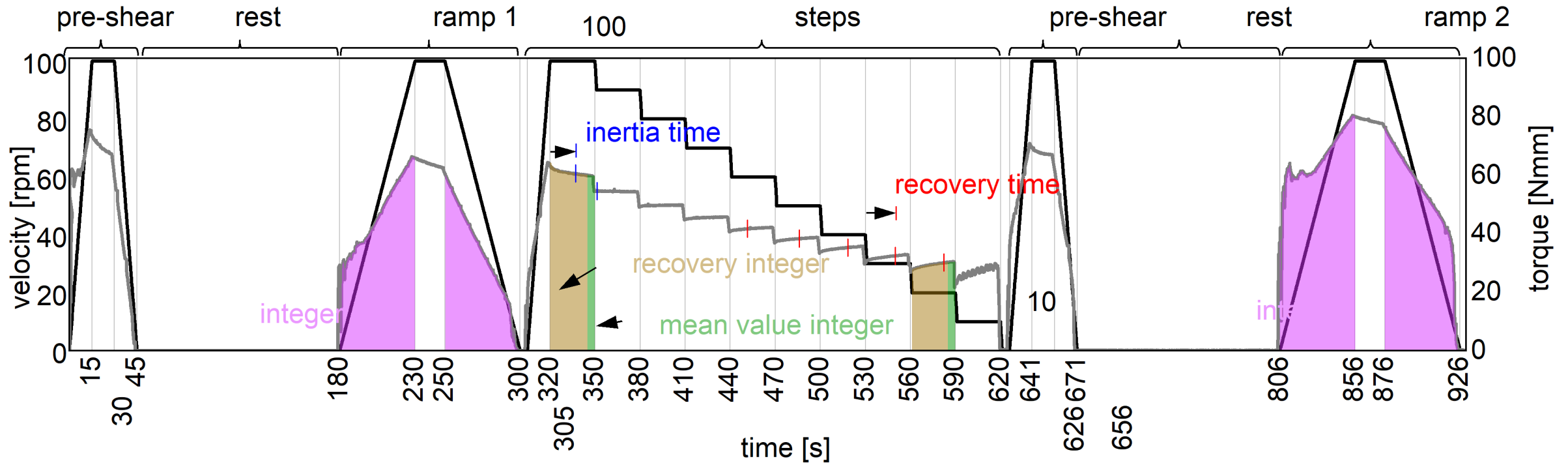
Thixotropy on a step profile

Inertia and recovery value



Thixotropy on a step profile

Hysteresis loop



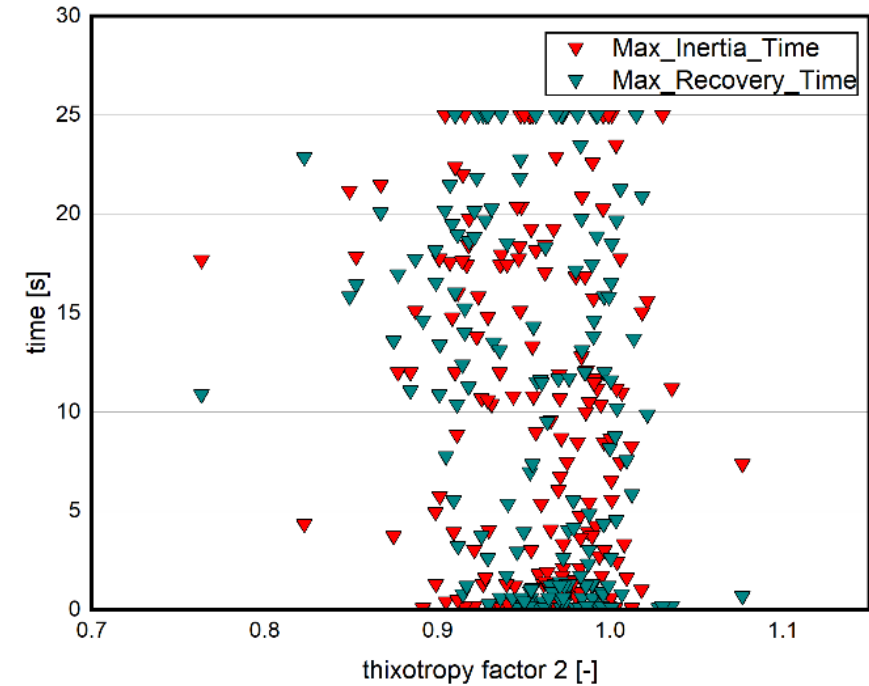
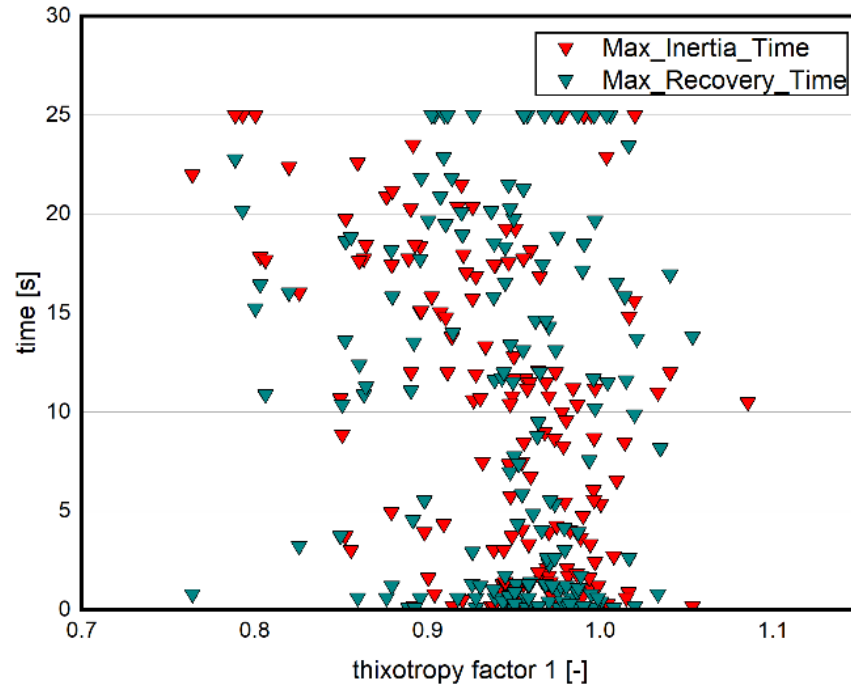
Inertia / recovery time: how fast does torque move towards mean value.

Threshold 1%

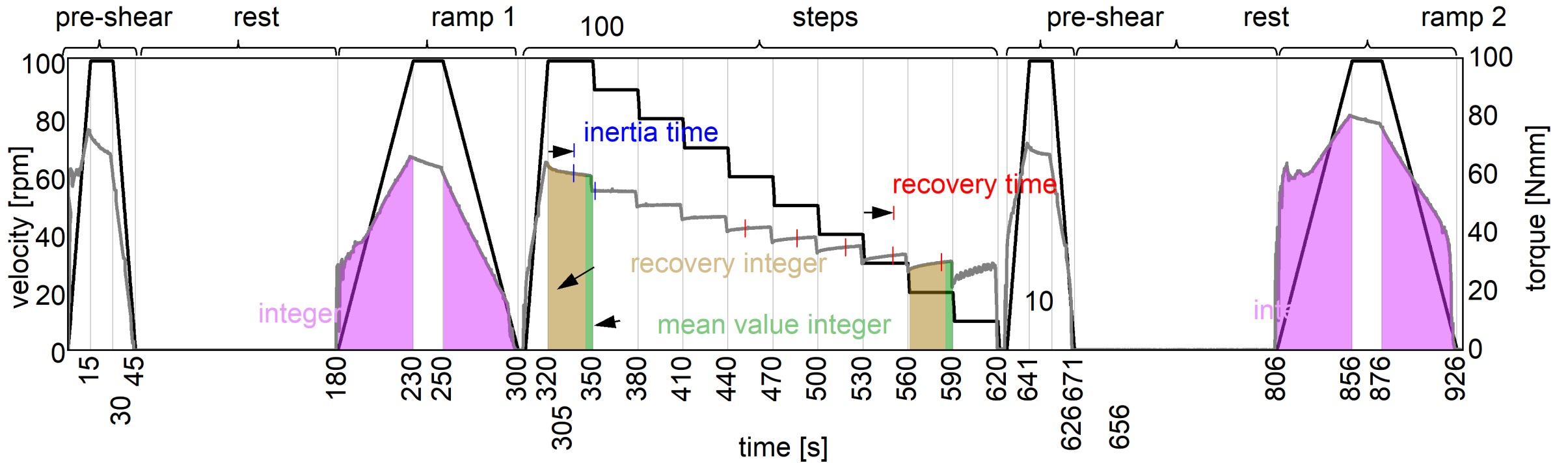
Minimum time within threshold: 1sec (~10data points)

Thixotropy on a step profile

Inertia and recovery time



Thixotropy on a step profile

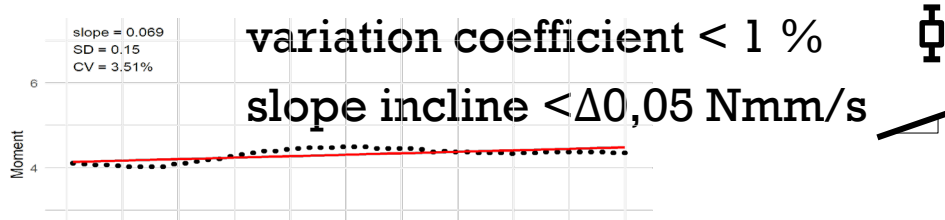
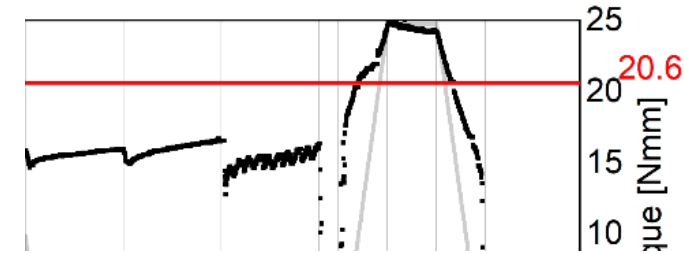


Ramp before steps
Step changes

Take Home Messages



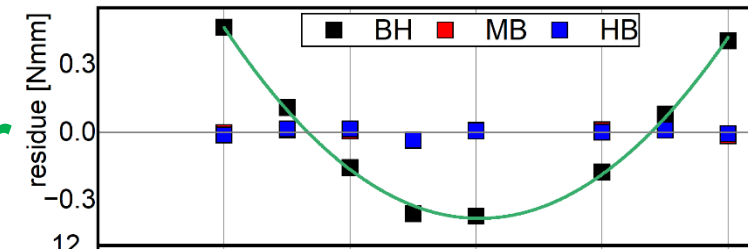
max RPM after steps check for data integrity



Equilibrium conditions via slope and variation coefficient

Flow model choice with Bingham residuum fit

$r^2 = 0.50$ > linear
< nonlinear



Thixotropy on step analysis as a “sidekick” unreliable



Thanks for your attention

www.unibw.de/werkstoffe-en